

1. ☒ This is a **FIRST** submission of items concerning a filing under 35 U.S.C. § 371.
2. ☐ This is a **SECOND** or **SUBSEQUENT** submission of items concerning a filing under 35 U.S.C. § 371.
3. ☐ This is an express request to begin national examination procedures (35 U.S.C. § 371(f)) at any time rather than delay examination until the expiration of the applicable time limit set in 35 U.S.C. § 371(b) and PCT Articles 22 and 39(I).
4. ☐ A translation of the International Application into English (35 U.S.C. § 371(c)(2)).
5. ☐ Drawings  
☐ Formal Figure(s) \_\_\_\_\_ on \_\_\_\_\_ sheet(s).
6. ☒ A copy of the International Application as filed (35 U.S.C. § 371(c)(2))  
☒ is transmitted herewith including: a title page; 14 page specification; 2 page(s) of claims (claims 1-6); 1 page abstract.  
☐ has been transmitted by the International Bureau.  
☐ is not required, as the application was filed in the United States Receiving Office (RO/US).

7. ☐ Amendments to the claims of the International Application under PCT Article 19 (35 U.S.C. § 371(c)(3))  
☐ are transmitted herewith (required only if not transmitted by the International Bureau).  
☐ have been transmitted by the International Bureau.  
☐ have not been made; however, the time limit for making such amendments has NOT expired.  
☐ have not been made and will not be made.
8. ☐ A translation of the amendments to the claims under PCT Article 19 (35 U.S.C. § 371(c)(3)).
9. ☒ A proper Demand for International Preliminary Examination was made by the 19th month from the earliest claimed priority date.  
☐ A copy of the Demand for International Preliminary Examination is enclosed.
10. ☐ An oath or declaration of the inventor(s) (35 U.S.C. § 371(c)(4)):  
☐ is enclosed (\_\_\_\_ pages).  
☐ a combined Declaration and Power of Attorney is enclosed (\_\_\_\_ pages).  
☒ is not enclosed. Applicant requests the Patent and Trademark Office to accept this application and accord a serial number and filing date as of the date this application is deposited with the U.S. Postal Service for Express Mail. Further, Applicant requests that the NOTICE OF MISSING PARTS-FILING DATE GRANTED be sent to the undersigned representative of Applicant.
11. ☒ Applicant hereby claims priority to:  
☒ International Application No.: PCT/KR99/00638 filed October 23, 1999.  
☒ Korean application No.: KR 1999/19193 filed May 27, 1999.
12. ☐ A translation of the annexes of the International Preliminary Examination Report under PCT Article 36 (35 U.S.C. § 371(c)(5)).
13. ☒ The entire disclosure of the International Application referred to above is considered to be part of the accompanying application and is hereby incorporated by reference herein.
14. ☐ Assignment Papers.  
☐ An assignment document is enclosed for recording (\_\_\_\_ pages).  
☐ Form PTO-1595 Assignment Recordation Cover Sheet (\_\_\_\_ page).
15. ☒ A Preliminary Amendment (7 pages).
16. ☒ A substitute specification for pages 1-14, 17 (16 pages).
17. ☒ A strikethrough version of specification and abstract (15 pages).
18. ☐ Power of Attorney  
☐ Is enclosed.  
☐ a combined Declaration and Power of Attorney is enclosed.
19. ☐ Information Disclosure Statement (IDS), including:  
☐ Form PTO-1449  
☐ Reference(s) marked according to Form PTO-1449.
20. ☒ Return Receipt Postcard
21. ☐ Small Entity Status  
☐ A small entity statement is enclosed.
22. ☐ Copy of PCT Form PCT/IB/338
23. ☐ Copy of International Request.

24. ☒ Copy of International Preliminary Examination Report.  
☐ A copy of the International Preliminary Examination Report in French.  
☐ English Translation of the International Preliminary Examination Report.

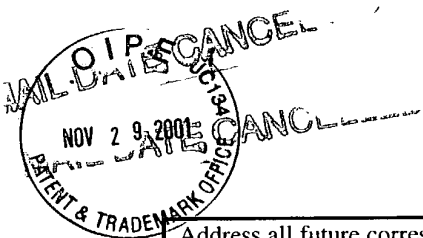
25. ☒ The following fees are submitted:

BASIC NATIONAL FEE (37 CFR § 1.492 (a) (1)-(5):				
<input type="checkbox"/> Neither international preliminary examination fee nor international search fee paid to USPTO and International Search Report not prepared by the EPO or JPO.....\$970.00				
<input checked="" type="checkbox"/> International preliminary examination fee not paid to USPTO but International Search Report prepared by the EPO or JPO.....\$890.00				
<input type="checkbox"/> International preliminary examination fee not paid to USPTO but international search fee paid to USPTO.....\$760.00				
<input type="checkbox"/> International preliminary examination fee paid to USPTO but all claims did not satisfy provisions of PCT Article 33(1)-(4).....\$670.00				
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ENTER APPROPRIATE BASIC NATIONAL FEE AMOUNT (as selected above):				\$890.00
Surcharge of \$130.00 for furnishing oath or declaration later than <input type="checkbox"/> 20 <input type="checkbox"/> 30 Months from the earliest claimed priority date (37 C.F.R. § 1.492(e)).				
CLAIMS	NUMBER FILED	NUMBER EXTRA	RATE	
Total claims	27 - 20 =	7	7 x \$18.00 =	126.00
Independent claims	3 - 3 =	0	x \$78.00 =	
MULTIPLE DEPENDENT CLAIM(S)			+ \$260.00 =	
TOTAL OF ABOVE CALCULATIONS:				\$1016.00
Reduction by 50% for Small Entity. A Small Entity Statement must be filed:				
SUBTOTAL:				\$1016.00
Processing fee of \$130.00 for furnishing the English translation later than <input type="checkbox"/> 20 <input type="checkbox"/> 30 Months from the earliest claimed priority date:				
TOTAL NATIONAL FEE:				
Fee for recording the enclosed assignment. The assignment must be accompanied by an appropriate cover sheet. \$40.00 per property:				
TOTAL FEES ENCLOSED:				

☒ A fee authorization in the amount of \$1016.00 is enclosed.

☐ Please charge my Deposit Account No. 50-1505/ in the amount of to cover the above fees.

☒ The Commissioner is hereby authorized to charge any other fees which may be required or credit any overpayment to Conley, Rose, & Tayon, P.C., Deposit Account No. 50-1505/5333-02400/EBM.



0998097980505  
JC10 Rec'd PCT/PTO 27 NOV 2001

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44,649

Date

11/27/01

**PATENT 5333-02400**

Title: A CATALYST FOR  
ETHYLENE HOMO- AND  
CO-POLYMERIZATION

**CERTIFICATE OF EXPRESS MAIL**  
**UNDER 37 C.F.R. §1.10**

"Express Mail" mailing label number EL893865091US  
DATE OF DEPOSIT: November 27, 2001

I hereby certify that this paper or fee is being deposited with the United States Postal Service "Express Mail Post Office to Addressee" service under 37 C.F.R. §1 10 on the date indicated above and is addressed to.

Commissioner for Patents  
Box Patent Application  
P.O. Box 2327  
Arlington, VA 22202

Derrick Brown

**PRELIMINARY AMENDMENT**

Commissioner for Patents  
P.O. Box 2327  
Arlington, VA 22202

Sir:

Please amend the above-captioned application as follows:

***In the Specification:***

Please replace pages 1-14 of the specification with pages 1-14 of the enclosed substitute sheets. Applicant has also submitted herewith a strikethrough version of the specification indicating the amendments.

Yang, et al.  
Atty. Dkt. No. 5333-02400

*In the Claims:*

Please cancel claims 1-6 without prejudice.

Please add the following claims.

7. (new) A solid titanium catalyst for homo-polymerization and co-polymerization of ethylene, wherein the catalyst is produced by:

preparing a magnesium compound solution by contacting a magnesium halide compound with an alcohol;

preparing a second solution by reacting the magnesium compound solution with an ester compound and a boron compound; and

reacting the second solution with a mixture of a titanium compound and a silicon compound to produce the solid titanium catalyst.

8. (new) The solid titanium catalyst of claim 7, wherein the produced solid titanium catalyst is further reacted with a second titanium compound.

9. (new) The solid titanium catalyst of claim 7, wherein the ester compound comprises an ester compound having at least one hydroxy group.

10. (new) The solid titanium catalyst of claim 7, wherein the ester compound comprises an unsaturated aliphatic ester having at least one hydroxy group.

11. (new) The solid titanium catalyst of claim 7, wherein the ester compound comprises 2-



boron compound having an alkoxy group.

18. (new) The solid titanium catalyst of claim 7, wherein the boron compound comprises the general formula  $BR^1_n(OR^2)_{3-n}$ , wherein  $R^1$  comprises a hydrocarbon having between 1 to 20 carbons or a halogen element, wherein  $R^2$  comprises a hydrocarbon having between 1 to 20 carbons, and wherein n comprises an integer between 0 and 2.
19. (new) The solid titanium catalyst of claim 7, wherein the boron compound comprises trimethyl borate, triethyl borate, tributyl borate, triphenyl borate, methylboron diethoxide, ethylboron diethoxide, ethylboron dibutoxide, butylboron dibutoxide, phenylboron diphenoxide, diethylboron ethoxide, dibutylboron ethoxide, diphenylboron phenoxide, diethoxyboron chloride, diethoxyboron bromide, diphenoxyboron chloride, ethoxyboron dichloride, ethoxyboron dibromide, butoxyboron dichloride, phenoxyboron dichloride, or ethylethoxyboron chloride.
20. (new) The solid titanium catalyst of claim 7, wherein the titanium compound comprises the general formula  $Ti(OR)_aX_{4-a}$ , wherein R comprises an alkyl group with 1 to 20 carbon atoms, wherein X comprises a halogen atom, and wherein a comprises an integer between 0 and 4.
21. (new) The solid titanium catalyst of claim 7, wherein the titanium compound comprises a titanium tetrahalide, wherein the titanium tetrahalide comprises  $TiCl_4$ ,  $TiBr_4$ , or  $TiI_4$ .
22. (new) The solid titanium catalyst of claim 7, wherein the titanium compound comprises an alkoxy-titanium trihalide, wherein the alkoxy-titanium trihalide comprises  $Ti(OCH_3)Cl_3$ ,  $Ti(OC_2H_5)Cl_3$ ,  $Ti(OC_2H_5)Br_3$ , or  $Ti(O(i-C_4H_9))Br_3$ .
23. (new) The solid titanium catalyst of claim 7, wherein the titanium compound comprises an alkoxy-titanium dihalide, wherein the alkoxy-titanium dihalide comprises  $Ti(OCH_3)_2Cl_2$ ,  $Ti(OC_2H_5)_2Cl_2$ ,  $Ti(OC_2H_5)_2Br_2$ , or  $Ti(O(i-C_4H_9))_2Cl_2$ .



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24. (new) The solid titanium catalyst of claim 7, wherein the titanium compound comprises a tetraalkoxy-titanium compound, wherein the tetraalkoxy-titanium compound comprises  $\text{Ti}(\text{OCH}_3)_4$ ,  $\text{Ti}(\text{OC}_2\text{H}_5)_4$ , or  $\text{Ti}(\text{OC}_4\text{H}_9)_4$ .
25. (new) The solid titanium catalyst of claim 7, wherein the silicon compound comprises the general formula  $\text{R}_n\text{SiCl}_{4-n}$ , wherein R comprises hydrogen, or R comprises an alkyl group, an alkoxy group, a haloalkyl group, or an aryl group having 1 to 10 carbon atoms, or R comprises a halosilyl group or a halosilyl alkyl group having 1 to 8 carbon atoms, and wherein n comprises an integer between 0 and 4.
26. (new) The solid titanium catalyst of claim 7, wherein the silicon compound comprises silicon tetrachloride.
27. (new) The solid titanium catalyst of claim 7, wherein the silicon compound comprises a trichlorosilane, wherein the trichlorosilane comprises methyltrichlorosilane, ethyltrichlorosilane, or phenyl-trichlorosilane.
28. (new) The solid titanium catalyst of claim 7, wherein the silicon compound comprises a dichlorosilane, wherein the dichlorosilane comprises dimethyldichlorosilane, diethyldichlorosilane, diphenyldichlorosilane, or methylphenyldichlorosilane.
29. (new) The solid titanium catalyst of claim 7, wherein the silicon compound comprises trimethylchlorosilane.
30. (new) The solid titanium catalyst of claim 7, wherein the ester compound comprises 2-hydroxyethyl methacrylate, wherein the boron compound comprises trimethyl borate, wherein the titanium compound comprises titanium tetrachloride, and wherein the silicon compound

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comprises silicon tetrachloride.

31. (new) The solid titanium catalyst of claim 7, wherein an amount of the mixture of the titanium compound and the silicon compound is between about 0.1 mol per mole of the magnesium halide compound and about 200 mol per mole of the magnesium halide compound, and wherein the molar ratio of the titanium compound to the silicon compound in the mixture is between about 0.05 and about 0.95.

32. (new) A method for producing a solid titanium catalyst, comprising:

preparing a magnesium compound solution by contacting a magnesium halide compound with an alcohol;

preparing a second solution by reacting the magnesium compound solution with an ester compound and a boron compound; and

reacting the second solution with a mixture of a titanium compound and a silicon compound to produce the solid titanium catalyst.

33. (new) A solid titanium catalyst for homo-polymerization and co-polymerization of ethylene, wherein the catalyst is produced by:

preparing a magnesium compound solution by contacting a magnesium halide compound with an alcohol;

preparing a second solution by reacting the magnesium compound solution with an ester compound having at least one hydroxy group and a boron compound having an alkoxy group; and

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reacting the second solution with a mixture of a titanium compound and a silicon compound to produce the solid titanium catalyst.

***In the Abstract:***

Please replace the abstract with the enclosed substitute sheet. Applicant has also submitted herewith a strikethrough version of the abstract indicating the amendments.

It is believed that no fees are due in connection with the filing of this Preliminary Amendment. However, if any fees are due, the Assistant Commissioner is hereby authorized to deduct said fees from Conley, Rose & Tayon Deposit Account No. 50-1505/5333-02400/EBM.

Respectfully submitted,



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Patent Agent for Applicant

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Date: 11/27/01

**BACKGROUND OF THE INVENTION**

## 1. FIELD OF THE INVENTION

The present invention relates to a catalyst for homo-polymerization or co-polymerization of ethylene, or more particularly to a good-activity titanium solid complex catalyst supported in a carrier containing magnesium, the catalyst being capable of producing polymers of high bulk density with a narrow particle distribution and low contents of fine particles.

## 2. DESCRIPTION OF THE RELATED ART

Catalysts containing magnesium for polymerization or co-polymerization of ethylene are known to have very good catalytic activities and to accord good bulk density, which are suitable for liquid-phase or gas-phase polymerization. By liquid phase polymerization of ethylene, it denotes the polymerization process performed in such medium of bulk ethylene, isopentane, or hexane, and as for the important characteristics of the catalyst used in the process, they are as follows: high activity, bulk density, the amount of molecules of low molecular weight dissolved in a medium, particle distribution of polymers, the amount of fine particles, and so on.

Many of the titanium-based catalysts containing magnesium for olefin polymerization, and the manufacturing methods thereof have been reported. Especially, many processes making use of magnesium solutions to obtain olefin polymerization catalysts of good bulk density have been known. There is a means of obtaining a magnesium solution by reacting magnesium compounds with such electron donors as alcohol, amine, cyclic ether, or organic carboxylic acid in the presence of a hydrocarbon solvent. As for the cases of use of alcohol, they are disclosed in US Patent Nos. 4,330,649, and 5,106,807. Further, the methods for production of catalysts containing magnesium by reacting a magnesium solution with a halide compound such as titanium tetrachloride are well known. Such catalysts provide good bulk density, but there is much yet to be improved with respect to their catalytic activity and bulk density. Meanwhile, when the polymerization is carried out by means of using such catalysts, the resultant polymers have large amounts of fine powder with a broad particle size distribution and low bulk density. As such, there are serious defects with respect to productivity and handling at the time of processing.

To solve these problems, US Patent Nos. 3,953,414 and 4,111,835 disclosed a process for making catalysts for production of globular polymers with a very large average particle size by means of spray-drying magnesium dichloride hydrates. These processes, however, require much production facilities for catalysts such as spray-drying equipment and others, and the resultant catalysts have the disadvantages of low activities. Further, due to the existence of very large particles in polymers, there may arise problems at the time of the melting process.

### SUMMARY OF THE INVENTION

As shown above, there is a need for the development of a new catalyst for homo-polymerization or co-polymerization of ethylene for producing polymers with the following conditions: simple manufacturing process, high polymerization activity, high bulk density for polymers by means of controlling the catalyst particles, and in particular narrow particle distribution with few fine particles. In the present invention, therefore, it is intended to provide a method for producing, from low-cost compounds via a simple process, a catalyst having an excellent catalytic activity, capable of producing polymers of high bulk density with narrow particle distribution and few fine particles. Further, the specific production process of catalysts and the steps thereof as disclosed in the present invention have never been reported in the prior art.

Consequently, the objective of the present invention is to provide a catalyst for homo-polymerization or co-polymerization of ethylene, said catalyst having good catalytic activity, capable of producing polymers of high bulk density, with narrow particle distribution and few fine particles.

Another objective of the present invention is to provide a simple process for producing a catalyst for homo-polymerization or co-polymerization of ethylene.

Still other objectives and the utility of the present invention will become apparent as references are made with respect to the following descriptions and the claims thereto.

# **DETAILED DESCRIPTION OF THE PREFERRED EMBODIMENTS**

The catalyst of good catalytic activity, capable of producing polymers having narrow particle distribution and high bulk density with few fine particles as provided in the present invention, is produced by a simple yet efficient manufacturing process, which comprises (i) preparing a magnesium solution by contact-reacting a magnesium halide compound, with an alcohol, (ii) reacting the same with an ester compound containing at least one hydroxy group and a boron compound containing an alkoxy group, and (iii) producing a solid titanium catalyst by adding a titanium compound and a silicon compound.

Types of magnesium halide compounds used in the present invention are as follows: magnesium dihalides such as magnesium chloride, magnesium iodide, magnesium fluoride, and magnesium bromide; alkylmagnesium halides such as methylmagnesium halide, ethylmagnesium halide, propylmagnesium halide, butylmagnesium halide, isobutylmagnesium halide, hexylmagnesium halide, amylmagnesium halide, alkoxymagnesium halides such as methoxymagnesium halide, ethoxymagnesium halide, isopropoxymagnesium halide, butoxymagnesium halide, octoxymagnesium halide; and aryloxymagnesium halides such as phenoxymagnesium halide and methyl-phenoxymagnesium halide. Of the above magnesium compounds, two or more compounds can be used in a mixture. Further, the above magnesium compounds can be effectively used in the form of a complex compound with other metals.

Of the compounds listed above, some can be represented by a simple formula, but the others cannot be so represented depending on the production methods of magnesium compounds. In the latter cases, it can be generally regarded as a mixture of some of the listed compounds. For example, the following compounds can be used in the present invention: such compounds obtained by reacting magnesium compounds with polysiloxane compounds, silane compounds containing halogen, ester, or alcohol; and such compounds obtained by reacting magnesium metals with alcohol, phenol, or ether in the presence of halosilane, phosphorus pentachloride, or thionyl chloride. However, the preferable magnesium compounds are magnesium halides, especially magnesium chloride or alkylmagnesium chloride, preferably those having an alkyl group of 1 ~ 10 carbons; alkoxymagnesium chlorides, preferably those having 1 ~ 10 carbons; and aryloxymagnesium chlorides, preferably those having 6 ~ 20 carbons. The magnesium

solution used in the present invention is made by dissolving the aforementioned compounds with alcohol as a solvent in the presence or absence of a hydrocarbon solvent.

As to the types of hydrocarbon solvents used in the present invention, they include aliphatic hydrocarbons such as pentane, hexane, heptane, octane, decane, and kerosene; alicyclic hydrocarbons such as cyclopentane, methycyclopentane, cyclohexane, and methylcyclohexane; aromatic hydrocarbons such as benzene, toluene, xylene, ethylbenzene, cumene, and cymene; and halogenated hydrocarbons such as dichloropropane, dichloroethylene, trichloroethylene, carbon tetrachloride, and chlorobenzene.

When a magnesium compound is converted into a magnesium solution, alcohol is used in the presence or absence of the aforementioned hydrocarbons. The types of alcohol include those containing 1 ~ 20 carbon atoms such as methanol, ethanol, propanol, butanol, pentanol, hexanol, octanol, decanol, dodecanol, octadecyl alcohol, benzyl alcohol, phenylethyl alcohol, isopropyl benzyl alcohol, and cumyl-alcohol, although alcohols containing 1 ~ 12 carbon atoms are preferable. The average size of a target catalyst and its particle distribution can vary according to the type of alcohol, the total contents, types of magnesium compounds, and the ratio of magnesium to alcohol, etc. Nevertheless, the total amount of alcohol required to obtain the magnesium solution is at least 0.5 mol per each mole of the magnesium compound, preferably about 1.0 ~ 20 mol, or more preferably about 2.0 ~ 10 mol.

The reaction of a magnesium compound with alcohol for producing magnesium solution is preferably carried out in the presence of hydrocarbon. The reaction temperature, while variable depending on the type and the amount of alcohol, is at least -25°C, preferably -10 ~ 200°C, or more preferably about 0 ~ 150°C. It is preferable to carry out the reaction for about 15 minutes ~ 5 hours, preferably for about 30 minutes ~ 4 hours.

Of the electron donors used in the present invention, the ester compounds containing at least one hydroxy group include unsaturated aliphatic acid esters having at least one hydroxy group such as, 2-hydroxy ethylacrylate, 2-hydroxy ethylmethacrylate, 2-hydroxypropyl acrylate, 2-hydroxypropylmethacrylate, 4-hydroxy butylacrylate, pentaerithritol triacrylate; aliphatic monoesters or polyesters containing at least one hydroxy group such as 2-hydroxy ethyl acetate, methyl 3-hydroxy butylate, ethyl 3-hydroxy butylate, methyl 2-hydroxy isobutylate, ethyl

For the boron compound containing an alkoxy group, the other electron donor in the present invention, a compound having a general formula of  $\text{BR}^1_n(\text{OR}^2)_{3-n}$  (here,  $\text{R}^1$  represents a hydrocarbon having 1 ~ 20 carbons or a halogen element,  $\text{R}^2$  for a hydrocarbon having 1 ~ 20 carbons, and  $n$  for an integer of 0 ~ 2) is preferable. More specifically, it includes trimethyl borate, triethyl borate, tributyl borate, triphenyl borate, methylboron diethoxide, ethylboron diethoxide, ethylboron dibutoxide, butylboron dibutoxide, phenylboron phenoxide, diethylboron ethoxide, dibutylboron ethoxide, diphenylboron phenoxide, diethoxyboron chloride, diethoxyboron bromide, diphenoxyboron chloride, ethoxyboron dichloride, ethoxyboron dibromide, butoxyboron dichloride, phenoxyboron dichloride, and ethylethoxyboron chloride. The amount of such compound should be 0.005 mol per mole of magnesium, or more preferably 0.05 ~ 2 mol per mole of magnesium.

As for the temperature for the contact-reaction of a magnesium solution, an ester compound containing at least one hydroxy group, and an alkoxy boron compound, the temperature of 0 ~ 100°C is appropriate, or more preferably 10 ~ 70°C.

In the process, the catalyst particles are recrystallized by reacting the magnesium compound solution with a mixture of a liquid titanium compound of a general formula of  $\text{Ti}(\text{OR})_a\text{X}_{4-a}$  (R-stands for an alkyl group with 1 ~ 10 carbons; X for a halogen atom; and "a" for a



natural number of 0 to 4) and a silicon compound of a general formula of  $R_nSiCl_{4-n}$  (here R stands for hydrogen; or an alkyl, alkoxy, haloalkyl, or aryl group having 1 to 10 carbons; or a halosilyl or halosilyl alkyl group having 1 to 8 carbons;  $n = 0-3$ ). The types of titanium compounds which satisfy the general formula of  $Ti(OR)_aX_{4-a}$  include titanium tetrahalide such as  
 5  $TiCl_4$ ,  $TiBr_4$ , and  $TiI_4$ ; alkoxy titanium trihalide such as  $Ti(OCH_3)Cl_3$ ,  $Ti(OC_2H_5)Cl_3$ ,  $Ti(OC_2H_5)Br_3$ , and  $Ti(O(i-C_4H_9)Br_3$ ; alkoxy titanium dihalide compounds such as  $Ti(OCH_3)_2Cl_2$ ,  $Ti(OC_2H_5)_2Cl_2$ ,  $Ti(O(i-C_4H_9)_2Cl_2$ , and  $Ti(OC_2H_5)_2Br_2$ ; and tetra-alkoxy titaniums such as  $Ti(OCH_3)_4$ ,  $Ti(OC_2H_5)_4$ , and  $Ti(OC_4H_9)_4$ . A mixture of the above titanium compounds can also be used in the present invention. However, the preferable titanium compounds are those  
 10 containing halogen, or more preferably titanium tetrachloride.

The types of silicon compounds satisfying the above general formula of  $R_nSiCl_{4-n}$  include silicon tetrachloride; trichlorosilanes such as methyltrichlorosilane, ethyltrichlorosilane, phenyltrichlorosilane; dichlorosilanes such as dimethyldichlorosilane, diethyldichlorosilane, di-  
 15 phenyldichlorosilane, and methylphenyldichlorosilane; monochlorosilanes such as trimethylchlorosilane; and a mixture of these silicon compounds can also be used in the present invention, or more preferably silicon tetrachloride can be used.

The amount of the mixture of a titanium compound and a silicon compound used during the  
 20 re-crystallization of the magnesium compound solution is appropriately 0.1 ~ 200 mol per mole of the magnesium halide compound, preferably 0.1 ~ 100 mol, or more preferably 0.2 ~ 80 mol. The molar ratio of a titanium compound to a silicon compound in the mixture is appropriately 0.05 ~ 0.95, or more preferably 0.1 ~ 0.8. When the magnesium compound solution is reacted with the mixture of a titanium compound and a silicon compound, the shape  
 25 and the size of the resultant re-crystallized solid constituents vary a great deal according to the reaction conditions. In order to obtain the target size of the catalyst and the size and distribution of the polymers, as intended by the present invention, it is advantageous to maintain the above mixture amounts for said titanium and silicon compounds, as well as their mix ratios. If it is outside of the above range, it will be difficult to obtain the results as intended. The reaction of  
 30 the magnesium compound with the mixture of a titanium compound and a silicon compound should be carried out preferably at a sufficiently low temperature to result in formation of solid constituents. More preferably, the reaction should be carried out by contact-reaction at  $-70 \sim$

The particles of the solid catalysts obtained during the above process can be further reacted with titanium compounds. These titanium compounds are titanium halides, and alkoxy titanium halide with an alkoxy functional group of 1 ~ 20 carbons. At times, a mixture of these compounds can also be used. Of these compounds, however, titanium halide and an alkoxy titanium halide compound having an alkoxy functional group of 1~8 carbons can be appropriately used, or more preferably titanium tetrahalide can be used.

Further, the solid complex titanium catalysts produced during the process of the present invention can be utilized during homo-polymerization or co- polymerization of ethylene. In particular, the catalyst is used in homo-polymerization of ethylene, and also in co-polymerization of ethylene and  $\alpha$  -olefin such as propylene, 1-butene, 1-pentene, 1-methyl-1-pentene, or 1-hexene having three or more carbons.

The polymerization reaction in the presence of the catalyst of the present invention is carried out by means of using (i) a solid complex titanium catalyst of the present invention, comprising magnesium, titanium, halogen, and electron donors, and (ii) a cocatalyst comprising, compounds of organic metals of Groups II and III of the Periodic Table.

The solid complex titanium catalyst constituents of the present invention can be used in pre-polymerization of ethylene or  $\alpha$ -olefin prior to the use in the aforementioned polymerization reaction. The pre-polymerization can be carried out in the presence of a hydrocarbon solvent such as hexane, at a sufficiently low temperature, with ethylene or  $\alpha$ -olefin under pressure, in the presence of the above catalyst constituents and such an organic aluminum compound as triethylaluminum. Pre-polymerization, by maintaining the shape of the catalyst by surrounding the catalyst particles with polymers, is helpful in producing food-quality post-polymerization shape of the polymers. The weight ratio of the polymers to the catalysts after pre-polymerization is ordinarily 0.1 : 1 to 20 : 1.

The organometallic compound in the present invention can be represented by a general formula of  $MR_n$ , wherein, M stands for a metal constituent of Group II or IIIA in the Periodic Table, such as magnesium, calcium, zinc, boron, aluminum, and gallium, R for an alkyl group with 1 ~ 20 carbons, such as a methyl, ethyl, butyl, hexyl, octyl, or decyl group, and n for the atomic value of the metal constituent. As for more preferable organometallic compounds, trialkyl aluminum having an alkyl group of 1 ~ 6 carbons, such as triethylaluminum and triisobutylaluminum, or the mixture thereof can be utilized. On occasions, an organic aluminum compound having one or more halogen or hydride groups, such as ethylaluminum dichloride, diethylaluminum chloride, ethyl-aluminum sesqui-chloride, or diisobutylaluminum hydride can also be used.

As for the polymerization reaction, it is possible to carry out either gas phase or bulk polymerization in the absence of an organic solvent, or liquid slurry polymerization in the presence of an organic solvent. These polymerization methods, however, are carried out in the absence of oxygen, water, or other compounds that may act as catalytic poison.

The concentration of the solid complex titanium compound (i) with respect to the polymerization system, in the case of a liquid phase slurry polymerization, is approximately 0.001 ~ 5 mmol in terms of the titanium atom of the catalyst per one liter of the solvent, or more preferably approximately 0.001 ~ 0.5 mmol. As for the solvent, the following compounds or the mixtures thereof can be used: alkanes or cycloalkanes such as pentane, hexane, heptane, n-octane, isooctane, cyclohexane, or methylcyclohexane; alkylaromatic such as toluene, xylene, ethylbenzene, isopropylbenzene, ethyltoluene, n-propylbenzene, or diethylbenzene; and halogenated aromatics such as chlorobenzene, chloronaphthalene, or ortho-dichlorobenzene.

In the case of gas phase polymerization, the amount of the solid complex titanium catalyst (i) should be approximately 0.001 ~ 5 mmol in terms of the titanium atom of the catalyst per one liter of the polymerization reactant, preferably approximately 0.001 ~ 1.0 mmol, or more preferably approximately 0.01 ~ 0.5 mmol.

The preferable concentration of the organometallic compound (ii) is about 1 - 2,000 mol, as calculated by the aluminum atoms, per mole of the titanium atoms in the catalyst (i), or more preferably about 5 ~ 500 mol.

To secure a good reaction rate of polymerization, the polymerization herein is carried out at a sufficiently good temperature, regardless of the polymerization manufacturing process. Generally, the temperature of approximately 20 ~ 200°C is appropriate, or more preferably approximately 20 ~ 95°C. The appropriate pressure of monomers at the time of polymerization is the atmospheric to 100 atm, or more preferably 2 ~ 50 atm.

In the present invention, the changes in the molecular weight according to the amount of hydrogen at the time of polymerization are shown as a melt index (ASTM D 1238), the index generally known in the art. The value of the melt index generally becomes greater as the molecular weight decreases.

The products obtained by the method of polymerization of the present invention are solid ethylene homogeneous polymers or the copolymers of ethylene and  $\alpha$ -olefin, which have excellent bulk density and fluidity. Since the polymer yields are sufficiently good, there is no need for the removal of the catalyst residues.

The present invention is further described by means of the examples and comparative examples as below but should not be confined or limited to these examples.

#### Example 1

##### Production of catalyst

A solid complex titanium catalyst was produced by means of the following three steps:

##### (i) Step: Production of magnesium solution

Into a 1.0L reactor equipped with a mechanical stirrer, replaced with nitrogen atmosphere, 9.5 g of  $MgCl_2$  and 400 ml of decane were placed therein. After they were

stirred at 300 rpm, 60 ml of 2-ethyl hexanol was added thereto. The temperature was raised to 120 °C, and then the reaction was allowed to continue for three hours. The homogenous solution, which was obtained after the reaction, was cooled to room temperature (25°C).

5

(ii) Step : Contact-reaction of a magnesium solution, an ester containing a hydroxy group and an alkoxy boron compound

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To the magnesium solution, cooled to room temperature as above, 1.2 ml of 2-hydroxyethyl methacrylate and 5.1 ml of trimethyl borate were added, and then the reaction was allowed to continue for an hour.

(iii) Step : Treatment of a mixture of a titanium compound and a silicon compound

15

Into the above solution, a solution mixture of 30 ml of titanium tetrachloride and 30 ml of silicon tetrachloride was dripped thereto for one hour at room temperature (25°C). After the completion of the dripping process, the temperature of the reactor was raised to 80°C while stirring, after which was maintained at that temperature for one hour. After stopping the stirring, the supernatant of the solution was removed, and to the remaining solid layer was added 300 ml of decane and 100 ml of titanium tetrachloride in sequence. There, the temperature was raised to 100°C and maintained thereat for two hours. After the reaction, the reactor was cooled to room temperature and the washing of the resulting solid product with 400ml of hexane was repeated until the removal of free unreacted titanium chloride. The titanium content of the solid catalyst so produced was 3.8%.

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#### Polymerization

30

A 2-L good-pressure reactor was dried in an oven and assembled while still hot. In order to make the inside of the reactor nitrogen atmosphere, nitrogen and vacuum were alternatively manipulated three times in the reactor. To the reactor was added 1,000 ml of n-hexane, after which 2 mmols of triethylaluminum and a solid catalyst by 0.03 mmol in terms of the titanium atoms were added thereto. Then, 500 ml of hydrogen was added. The temperature was raised to 80°C while stirring at 700 rpm. The pressure of ethylene was adjusted

to 80 psi, and the polymerization was allowed to continue for an hour. After the polymerization, the temperature of the reactor was lowered to room temperature, and a large amount of ethanol was added to stop the polymerization. The polymer thus produced was collected by separation and was dried in an oven at 50°C for at least six hours, whereby polyethylene was obtained in the form of white powder.

The polymerization activity (kg of polyethylene divided by mmol of Ti) was calculated as the weight (kg) ratio of the polymer as produced per the amount of the catalysts so used (mmol of Ti). The results of the polymerization are shown in Table 1, together with the bulk density (g/ ml) of the polymers, the melt index (g/10 minutes), and particle size distribution of the polymers.

#### Example 2

In Step (ii) of Example 1, 1.2 ml of 2-hydroxyethyl methacrylate and 7.7 ml of trimethyl borate were used for the production of the catalyst. The titanium content of the catalyst thus produced was 3.4 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

#### Example 3

In Step (ii) of Example 1, 1.2 ml of 2-hydroxyethyl methacrylate and 7.6 ml of triethyl borate were used for the production of the catalyst. The titanium content of the catalyst thus produced was 3.5 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

#### Example 4

In Step (ii) of Example 1, 1.2 ml of 2-hydroxyethyl methacrylate and 11.4 ml of triethyl borate were used for the production of the catalyst. The titanium content of the catalyst thus produced was 3.4 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

Example 5

In Step (ii) of Example 1, 1.2 ml of 2-hydroxyethyl methacrylate and 12.1 ml of tributyl borate were used for the production of the catalyst. The titanium content of the catalyst thus produced was 3.9 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

Example 6

In Step (ii) of Example 1, 1.2 ml of 2-hydroxyethyl methacrylate and 18.2 ml of tributyl borate were used for the production of the catalyst. The titanium content of the catalyst thus produced was 3.5 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

Example 7

In Step (ii) of Example 1, 1.2 ml of 2-hydroxyethyl methacrylate and 11.4 ml of triethyl borate were used, and in Step (iii) 40 ml of titanium tetrachloride and 20 ml of silicon tetrachloride were used for the production of the catalyst. The titanium content of the catalyst thus produced was 4.0 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

Example 8

In Step (ii) of Example 1, 1.2 ml of 2-hydroxyethyl methacrylate and 11.4 ml of triethyl borate were used, and in Step (iii) 20 ml of titanium tetrachloride and 40 ml of silicon tetrachloride were used for the production of the catalyst. The titanium content of the catalyst thus produced was 3.3 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

Comparative Example 1

In Step (ii) of Example 1, the catalyst was produced without 2-hydroxyethyl methacrylate or trimethyl borate. The titanium content of the catalyst thus produced was 3.9 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

Comparative Example 2

In Step (ii) of Example 1, 1.2 ml of 2-hydroxyethyl methacrylate was used alone, without trimethyl borate, for the production of the catalyst. The titanium content of the catalyst thus produced was 3.3 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

Comparative Example 3

In Step (ii) of Example 1, neither 2-hydroxyethyl methacrylate nor trimethyl borate was used, and in Step (iii) 60 ml of titanium tetrachloride was used for the production of the catalyst. The titanium content of the catalyst thus produced was 4.1 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

Comparative Example 4

In Step (ii) of Example 1, 1.2 ml of 2-hydroxyethyl methacrylate and 12.1 ml of tributyl borate were used, and in Step (iii) 60 ml of titanium tetrachloride was used for the production of the catalyst. The titanium content of the catalyst thus produced was 3.7 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.





**ABSTRACT**

The present invention relates to a catalyst for homo-polymerization or co-polymerization of ethylene, or more particularly to a solid complex titanium catalyst for homo-polymerization or  
5 co-polymerization of ethylene. The catalyst may be produced by preparing a magnesium solution by contact-reacting a magnesium halide compound with an alcohol. Reacting the solution with an ester compound and a boron compound. Then reacting the solution with a mixture of a titanium compound and a silicon compound.

~~A CATALYST FOR ETHYLENE HOMO- AND CO-POLYMERIZATION~~**BACKGROUND OF THE INVENTION**Technical Field1. FIELD OF THE INVENTION

The present invention relates to a catalyst for homo-polymerization or co-polymerization of ethylene, or more particularly to a good-activity titanium solid complex catalyst supported in a carrier containing magnesium, ~~said the~~ catalyst being capable of producing polymers of high bulk density with a narrow particle distribution and low contents of fine particles.

Background of the Invention2. DESCRIPTION OF THE RELATED ART

Catalysts containing magnesium for polymerization or co-polymerization of ethylene are known to have very good catalytic activities and to accord good bulk density, which are suitable for liquid-phase or gas-phase polymerization. By liquid phase polymerization of ethylene, it denotes the polymerization process performed in such medium of bulk ethylene, isopentane, or hexane, and as for the important characteristics of the catalyst used in the process, they are as follows: high activity, bulk density, the amount of molecules of low molecular weight dissolved in a medium, particle distribution of polymers, the amount of fine particles, and so on.

Many of the titanium-based catalysts containing magnesium for olefin polymerization, and the manufacturing methods thereof have been reported. Especially, many processes making use of magnesium solutions to obtain olefin polymerization catalysts of good bulk density have been known. There is a means of obtaining a magnesium solution by reacting magnesium compounds with such electron donors as alcohol, amine, cyclic ether, or organic carboxylic acid in the presence of a hydrocarbon solvent. As for the cases of use of alcohol, they are disclosed in US Patent Nos. 4,330,649, and 5,106,807. Further, the methods for production of catalysts containing magnesium by reacting a magnesium solution with a ~~halogenated compound~~halide compound such as titanium tetrachloride are well known. Such catalysts provide good bulk density, but there is much yet to be improved with respect to their catalytic activity and bulk density. Meanwhile, when the polymerization is carried out by means of using such catalysts, the resultant polymers have large amounts of fine powder with a broad particle size distribution

and low bulk density. As such, there are serious defects with respect to productivity and handling at the time of processing.

To solve these problems, US Patent Nos. 3,953,414 and 4,111,835 disclosed a process for making catalysts for production of globular polymers with a very large average particle size by means of spray-drying magnesium dichloride hydrates. These processes, however, require much production facilities for catalysts such as spray-drying equipment and others, and the resultant catalysts have the disadvantages of low activities. Further, due to the existence of very large particles in polymers, there may arise problems at the time of the melting process.

## Summary of the InventionSUMMARY OF THE INVENTION

As shown above, there is a need for the development of a new catalyst for homopolymerization or co-polymerization of ethylene for producing polymers with the following conditions: simple manufacturing process, high polymerization activity, high bulk density for polymers by means of controlling the catalyst particles, and in particular narrow particle distribution with few fine particles. In the present invention, therefore, it is intended to provide a method for producing, from low-cost compounds via a simple process, a catalyst having an excellent catalytic activity, capable of producing polymers of high bulk density with narrow particle distribution and few fine particles. Further, the specific production process of catalysts and the steps thereof as disclosed in the present invention have never been reported in the prior art.

Consequently, the objective of the present invention is to provide a catalyst for homopolymerization or co-polymerization of ethylene, said catalyst having good catalytic activity, capable of producing polymers of high bulk density, with narrow particle distribution and few fine particles.

Another objective of the present invention is to provide a simple process for producing a catalyst for homo-polymerization or co-polymerization of ethylene.

Still other objectives and the utility of the present invention will become ~~bulk-apparent~~ apparent as references are made with respect to the following descriptions and the claims thereto.

~~Detailed Description of the Preferred Embodiments~~ DETAILED DESCRIPTION OF THE  
PREFERRED EMBODIMENTS

The catalyst of good catalytic activity, capable of producing polymers having narrow  
 5 particle distribution and high bulk density with few fine particles as provided in the present  
 invention, is produced by a simple yet efficient manufacturing process, which comprises (i)  
 preparing a magnesium solution by contact-reacting a ~~halogenated-magnesium~~ magnesium halide  
 compound, with an alcohol, (ii) reacting the same with an ester compound containing at least one  
 hydroxy group and a boron compound containing an alkoxy group, and (iii) producing a solid  
 10 titanium catalyst by adding a titanium compound and a silicon compound.

Types of ~~halogenated-magnesium~~ magnesium halide compounds used in the present  
 invention are as follows: ~~di-halogenated-magnesium~~ magnesium dihalides such as magnesium  
 chloride, magnesium iodide, magnesium fluoride, and magnesium bromide; alkylmagnesium  
 15 halides such as methylmagnesium halide, ethylmagnesium halide, propylmagnesium halide,  
 butylmagnesium halide, isobutylmagnesium halide, hexylmagnesium halide, amylmagnesium  
 halide, alkoxymagnesium halides such as methoxymagnesium halide, ethoxymagnesium halide,  
 isopropoxymagnesium halide, butoxymagnesium halide, octoxymagnesium halide; and  
 aryloxymagnesium halides such as phenoxymagnesium halide and methyl-phenoxymagnesium  
 20 halide. Of the above magnesium compounds, two or more compounds can be used in a mixture.  
 Further, the above magnesium compounds can be effectively used in the form of a complex  
 compound with other metals.

Of the compounds listed above, some can be represented by a simple formula, but the  
 25 others cannot be so represented depending on the production methods of magnesium compounds.  
 In the latter cases, it can be generally regarded as a mixture of some of the listed compounds.  
 For example, the following compounds can be used in the present invention: such compounds  
 obtained by reacting magnesium compounds with polysiloxane compounds, silane compounds  
 containing halogen, ester, or alcohol; and such compounds obtained by reacting magnesium  
 30 metals with alcohol, phenol, or ether in the presence of halosilane, phosphorus pentachloride, or  
 thionyl chloride. However, the preferable magnesium compounds are magnesium halides,  
 especially magnesium chloride or alkylmagnesium chloride, preferably those having an alkyl  
 group of 1 ~ 10 carbons; alkoxymagnesium chlorides, preferably those having 1 ~ 10 carbons;

and aryloxymagnesium chlorides, preferably those having 6 ~ 20 carbons. The magnesium solution used in the present invention is made by dissolving the aforementioned compounds with alcohol as a solvent in the presence or absence of a hydrocarbon solvent.

5 As to the types of hydrocarbon solvents used in the present invention, they include aliphatic hydrocarbons such as pentane, hexane, heptane, octane, decane, and kerosene; alicyclic hydrocarbons such as ~~cyclobenzene, methylecyclobenzene~~ cyclopentane, methycyclopentane, cyclohexane, and methylcyclohexane; aromatic hydrocarbons such as benzene, toluene, xylene, ethylbenzene, cumene, and cymene; and halogenated hydrocarbons such as dichloropropane,  
10 dichloroethylene, trichloroethylene, carbon tetrachloride, and chlorobenzene.

When a magnesium compound is converted into a magnesium solution, alcohol is used in the presence or absence of the aforementioned hydrocarbons. The types of alcohol include those containing 1 ~ 20 carbon atoms such as methanol, ethanol, propanol, butanol, pentanol,  
15 hexanol, octanol, decanol, dodecanol, octadecyl alcohol, benzyl alcohol, phenylethyl alcohol, isopropyl benzyl alcohol, and cumyl-alcohol, although alcohols containing 1 ~ 12 carbon atoms are preferable. The average size of a target catalyst and its particle distribution can vary according to the type of alcohol, the total contents, types of magnesium compounds, and the ratio of magnesium to alcohol, etc. Nevertheless, the total amount of alcohol required to obtain the  
20 magnesium solution is at least 0.5 mol per each mole of the magnesium compound, preferably about 1.0 ~ 20 mol, or more preferably about 2.0 ~ 10 mol.

The reaction of a magnesium compound with alcohol for producing magnesium solution is preferably carried out in the presence of hydrocarbon. The reaction temperature, while variable  
25 depending on the type and the amount of alcohol, is at least -25°C, preferably -10 ~ 200°C, or more preferably about 0 ~ 150°C. It is preferable to carry out the reaction for about 15 minutes ~ 5 hours, preferably for about 30 minutes ~ 4 hours.

Of the electron donors used in the present invention, the ester compounds containing at  
30 least one hydroxy group include unsaturated aliphatic acid esters having at least one hydroxy group such as, 2-hydroxy ethylacrylate, 2-hydroxy ethylmethacrylate, 2-hydroxypropyl acrylate, 2-hydroxypropylmethacrylate, 4-hydroxy butylacrylate, pentaerithritol triacrylate; aliphatic monoesters or polyesters containing at least one hydroxy group such as 2-hydroxy ethyl acetate,

methyl 3-hydroxy butylate, ethyl 3-hydroxy butylate, methyl 2-hydroxy isobutylate, ethyl  
 2-hydroxy isobutylate, methyl 3-hydroxy-2-methyl propionate, 2,2-dimethyl-hydroxy  
 propionate, ethyl-6-hydroxy hexanoate, t-butyl-2-hydroxy isobutylate, diethyl-3-hydroxy  
 glutarate, ethyl lactate, isopropyl lactate, butyl isobutyl lactate, isobutyl lactate, ethyl mandelate,  
 5 dimethyl ethyl tartrate, ethyl tartrate, dibutyl tartrate, diethyl citrate, triethyl citrate,  
 ethyl-2-hydroxy-caproate, diethyl bis-(hydroxy methyl)malonate; aromatic esters having at least  
 one hydroxy group such as 2-hydroxy ethyl benzoate, 2-hydroxy ethyl salicylate, methyl-4-  
 (hydroxy methyl) benzoate, methyl-4-hydroxy benzoate, ethyl-3-hydroxy benzoate, 4-methyl  
 salicylate, ethyl salicylate, phenyl salicylate, propyl-4-hydroxy benzoate, phenyl-3-hydroxy  
 10 naphthanoate, monoethylene glycol monobenzoate, diethylene glycol benzoate, triethylene  
 glycol benzoate; alicyclic esters having at least one hydroxy group such as lactone, and others.  
 The amount of the ester compound containing at least one hydroxy group should be 0.001 ~ 5  
 mol per mole of magnesium, or preferably 0.01 ~ 2 mol per mole of magnesium.

15 For the boron compound containing an alkoxy group, the other electron donor in the  
 present invention, a compound having a general formula of  $BR^n_1(OR^2)_{3-n}$  (here,  $R^1$  represents a  
 hydrocarbon having 1 ~ 20 carbons or a halogen element,  $R^2$  for a hydrocarbon having 1 ~ 20  
 carbons, and n for an integer of 0 ~ 2) is preferable. More specifically, it includes trimethyl  
 borate, triethyl borate, tributyl borate, triphenyl borate, methylboron diethoxide, ethylboron  
 20 diethoxide, ethylboron dibutoxide, butylboron dibutoxide, phenylboron phenoxide, diethylboron  
 ethoxide, dibutylboron ethoxide, diphenylboron phenoxide, diethoxyboron chloride,  
 diethoxyboron bromide, diphenoxyboron ~~chloride~~ chloride, ethoxyboron dichloride, ethoxyboron  
 dibromide, butoxyboron dichloride, phenoxyboron dichloride, and ethylethoxyboron chloride.  
 The amount of such compound should be 0.005 mol per mole of magnesium, or more preferably  
 25 0.05 ~ 2 mol per mole of magnesium.

As for the temperature for the contact-reaction of a magnesium solution, an ester compound  
 containing at least one hydroxy group, and an alkoxy boron compound, the temperature of 0 ~  
 100°C is appropriate, or more preferably 10 ~ 70°C.

30 In the process, the catalyst particles are recrystallized by reacting the magnesium  
 compound solution with a mixture of a liquid titanium compound of a general formula of  
 $Ti(OR)_aX_{4-a}$  (R-stands for an alkyl group with 1 ~ 10 carbons; X for a halogen atom; and "a" for a

natural number of 0 to 4) and a silicon compound of a general formula of  $R_nSiCl_{4-n}$  (here R stands for hydrogen; or an alkyl, alkoxy, haloalkyl, or aryl group having 1 to 10 carbons; or a halosilyl or halosilyl alkyl group having 1 to 8 carbons;  $n = 0-3$ ). The types of titanium compounds which satisfy the general formula of  $Ti(OR)_aX_{4-a}$  include ~~4-halogenated titanium~~ titanium tetrahalide such as  $TiCl_4$ ,  $TiBr_4$ , and  $TiI_4$ ; ~~3-halogenated alkoxy-titanium~~ alkoxy titanium trihalide such as  $Ti(OCH_3)Cl_3$ ,  $Ti(OC_2H_5)Cl_3$ ,  $Ti(OC_2H_5)Br_3$ , and  $Ti(O(i-C_4H_9))Br_3$ ; ~~2-halogenated alkoxy-titanium~~ alkoxy titanium dihalide compounds such as  $Ti(OCH_3)_2Cl_2$ ,  $Ti(OC_2H_5)_2Cl_2$ ,  $Ti(O(i-C_4H_9))_2Cl_2$ , and  $Ti(OC_2H_5)_2Br_2$ ; and tetra-alkoxy titaniums such as  $Ti(OCH_3)_4$ ,  $Ti(OC_2H_5)_4$ , and  $Ti(OC_4H_9)_4$ . A mixture of the above titanium compounds can also be used in the present invention. However, the preferable titanium compounds are those containing halogen, or more preferably titanium tetrachloride.

The types of silicon compounds satisfying the above general formula of  $R_nSiCl_{4-n}$  include silicon tetrachloride; trichlorosilanes such as methyltrichlorosilane, ethyltrichlorosilane, phenyltrichlorosilane; dichlorosilanes such as ~~dimethylchlorosilane~~ dimethyldichlorosilane, diethyldichlorosilane, di-phenyldichlorosilane, and methylphenyldichlorosilane; monochlorosilanes such as trimethylchlorosilane; and a mixture of these silicon compounds can also be used in the present invention, or more preferably silicon tetrachloride can be used.

The amount of the mixture of a titanium compound and a silicon compound used during the re-crystallization of the magnesium compound solution is appropriately 0.1 ~ 200 mol per mole of the ~~halogenated-magnesium~~ magnesium halide compound, preferably 0.1 ~ 100 mol, or more preferably 0.2 ~ 80 mol. The molar ratio of a titanium compound to a silicon compound in the mixture is appropriately 0.05 ~ 0.95, or more preferably 0.1 ~ 0.8. When the magnesium compound solution is reacted with the mixture of a titanium compound and a silicon compound, the shape and the size of the resultant re-crystallized solid constituents vary a great deal according to the reaction conditions. In order to obtain the target size of the catalyst and the size and distribution of the polymers, as intended by the present invention, it is advantageous to maintain the above mixture amounts for said titanium and silicon compounds, as well as their mix ratios. If it is outside of the above range, it will be difficult to obtain the results as intended. The reaction of the magnesium compound with the mixture of a titanium compound and a silicon compound should be carried out preferably at a sufficiently low temperature to result in formation of solid constituents. More preferably, the reaction should be carried out by



contact-reaction at  $-70 \sim 70^{\circ}\text{C}$ , or most preferably at  $-50 \sim 50^{\circ}\text{C}$ . After the contact-reaction the reacting temperature is slowly raised for sufficient reaction for the duration of  $0.5 \sim 5$  hours at  $50 \sim 150^{\circ}\text{C}$ .

5 The particles of the solid catalysts obtained during the above process can be further reacted with titanium compounds. These titanium compounds are titanium halides, and ~~halogenated alkoxy titanium~~ alkoxy titanium halide with an alkoxy functional group of  $1 \sim 20$  carbons. At times, a mixture of these compounds can also be used. Of these compounds, however, titanium halide and ~~an halogenated alkoxy titanium~~ alkoxy titanium halide compound having an alkoxy  
10 functional group of  $1 \sim 8$  carbons can be appropriately used, or more preferably titanium tetrahalide can be used.

Further, the solid complex titanium catalysts produced during the process of the present invention can be utilized during homo-polymerization or co- polymerization of ethylene. In  
15 particular, the catalyst is used in homo-polymerization of ethylene, and also in co-polymerization of ethylene and  $\alpha$ -olefin such as propylene, 1-butene, 1-pentene, 1-methyl-1-pentene, or 1-hexene having three or more carbons.

The polymerization reaction in the presence of the catalyst of the present invention is  
20 carried out by means of using (i) a solid complex titanium catalyst of the present invention, comprising magnesium, titanium, halogen, and electron donors, and (ii) a cocatalyst comprising, compounds of organic metals of Groups II and III of the Periodic Table.

The solid complex titanium catalyst constituents of the present invention can be used in  
25 pre-polymerization of ethylene or  $\alpha$ -olefin prior to the use in the aforementioned polymerization reaction. The pre-polymerization can be carried out in the presence of a hydrocarbon solvent such as hexane, at a sufficiently low temperature, with ethylene or  $\alpha$ -olefin under pressure, in the presence of the above catalyst constituents and such an organic aluminum compound as triethylaluminum. Pre-polymerization, by maintaining the shape of the catalyst by surrounding  
30 the catalyst particle s with polymers, is helpful in producing food-quality post-polymerization shape of the polymers. The weight ratio of the polymers to the catalysts after pre-polymerization is ordinarily  $0.1 : 1$  to  $20 : 1$ .

The organometallic compound in the present invention can be represented by a general formula of  $MR_n$ , wherein, M stands for a metal constituent of Group II or IIIA in the Periodic Table, such as magnesium, calcium, zinc, boron, aluminum, and gallium, R for an alkyl group with 1 ~ 20 carbons, such as a methyl, ethyl, butyl, hexyl, octyl, or decyl group, and n for the atomic value of the metal constituent. As for more preferable organometallic compounds, trialkyl aluminum having an alkyl group of 1 ~ 6 carbons, such as triethylaluminum and triisobutylaluminum, or the mixture thereof can be utilized. On occasions, an organic aluminum compound having one or more halogen or hydride groups, such as ethylaluminum dichloride, diethylaluminum chloride, ethyl-aluminum sesqui-chloride, or diisobutylaluminum hydride can also be used.

As for the polymerization reaction, it is possible to carry out either gas phase or bulk polymerization in the absence of an organic solvent, or liquid slurry polymerization in the presence of an organic solvent. These polymerization methods, however, are carried out in the absence of oxygen, water, or other compounds that may act as catalytic poison.

The concentration of the solid complex titanium compound (i) with respect to the polymerization system, in the case of a liquid phase slurry polymerization, is approximately 0.001 ~ 5 mmol in terms of the titanium atom of the catalyst per one liter of the solvent, or more preferably approximately 0.001 ~ 0.5 mmol. As for the solvent, the following compounds or the mixtures thereof can be used: alkanes or cycloalkanes such as pentane, hexane, heptane, n-octane, isooctane, cyclohexane, or methylcyclohexane; alkylaromatic such as toluene, xylene, ethylbenzene, isopropylbenzene, ethyltoluene, n-propylbenzene, or diethylbenzene; and halogenated aromatics such as chlorobenzene, chloronaphthalene, or ortho-dichlorobenzene.

In the case of gas phase polymerization, the amount of the solid complex titanium catalyst (i) should be approximately 0.001 ~ 5 mmol in terms of the titanium atom of the catalyst per one liter of the polymerization reactant, preferably approximately 0.001 ~ 1.0 mmol, or more preferably approximately 0.01 ~ 0.5 mmol.

The preferable concentration of the organometallic compound (ii) is about 1 - 2,000 mol, as calculated by the aluminum atoms, per mole of the titanium atoms in the catalyst (i), or more preferably about 5 ~ 500 mol.

5 To secure a good reaction rate of polymerization, the polymerization herein is carried out at a sufficiently good temperature, regardless of the polymerization manufacturing process. Generally, the temperature of approximately 20 ~ 200°C is appropriate, or more preferably approximately 20 ~ 95°C. The appropriate pressure of monomers at the time of polymerization is the atmospheric to 100 atm, or more preferably 2 ~ 50 atm.

10 In the present invention, the changes in the molecular weight according to the amount of hydrogen at the time of polymerization are shown as a melt index (ASTM D 1238), the index generally known in the art. The value of the melt index generally becomes greater as the molecular weight decreases.

15 The products obtained by the method of polymerization of the present invention are solid ethylene homogeneous polymers or the copolymers of ethylene and  $\alpha$ -olefin, which have excellent bulk density and fluidity. Since the polymer yields are sufficiently good, there is no need for the removal of the catalyst residues.

20 The present invention is further described by means of the examples and comparative examples as below but should not be confined or limited to these examples.

#### Example 1

##### Production of catalyst

A solid complex titanium catalyst was produced by means of the following three steps:

##### (i) Step: Production of magnesium solution

Into a 1.0L reactor equipped with a mechanical stirrer, replaced with nitrogen atmosphere, 9.5 g of  $\text{MgCl}_2$  and 400 ml of decane were placed therein. After they were

stirred at 300 rpm, 60 ml of 2-ethyl hexanol was added thereto. The temperature was raised to 120 °C, and then the reaction was allowed to continue for three hours. The homogenous solution, which was obtained after the reaction, was cooled to room temperature (25°C).

5

(ii) Step : Contact-reaction of a magnesium solution, an ester containing a hydroxy group and an alkoxy boron compound

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To the magnesium solution, cooled to room temperature as above, 1.2 ml of 2-hydroxyethyl methacrylate and 5.1 ml of trimethyl borate were added, and then the reaction was allowed to continue for an hour.

(iii) Step : Treatment of a mixture of a titanium compound and a silicon compound

15

Into the above solution, a solution mixture of 30 ml of titanium tetrachloride and 30 ml of silicon tetrachloride was dripped thereto for one hour at room temperature (25°C). After the completion of the dripping process, the temperature of the reactor was raised to 80°C while stirring, after which was maintained at that temperature for one hour. After stopping the stirring, the supernatant of the solution was removed, and to the remaining solid layer was added 300 ml of decane and 100 ml of titanium tetrachloride in sequence. There, the temperature was raised to 100°C and maintained thereat for two hours. After the reaction, the reactor was cooled to room temperature and the washing of the resulting solid product with 400ml of hexane was repeated until the removal of free unreacted titanium chloride. The titanium content of the solid catalyst so produced was 3.8%.

20

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#### Polymerization

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A 2-L good-pressure reactor was dried in an oven and assembled while still hot. In order to make the inside of the reactor nitrogen atmosphere, nitrogen and vacuum were alternatively manipulated three times in the reactor. To the reactor was added 1,000 ml of n-hexane, after which 2 mmols of triethylaluminum and a solid catalyst by 0.03 mmol in terms of the titanium atoms were added thereto. Then, 500 ml of hydrogen was added. The temperature was raised to 80°C while stirring at 700 rpm. The pressure of ethylene was adjusted

to 80 psi, and the polymerization was allowed to continue for an hour. After the polymerization, the temperature of the reactor was lowered to room temperature, and a large amount of ethanol was added to stop the polymerization. The polymer thus produced was collected by separation and was dried in an oven at 50°C for at least six hours, whereby polyethylene was obtained in the form of white powder.

The polymerization activity (kg of polyethylene divided by mmol of Ti) was calculated as the weight (kg) ratio of the polymer as produced per the amount of the catalysts so used (mmol of Ti). The results of the polymerization are shown in Table 1, together with the bulk density (g/ ml) of the polymers, the melt index (g/10 minutes), and particle size distribution of the polymers.

#### Example 2

In Step (ii) of Example 1, 1.2 ml of 2-hydroxyethyl methacrylate and 7.7 ml of trimethyl borate were used for the production of the catalyst. The titanium content of the catalyst thus produced was 3.4 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

#### Example 3

In Step (ii) of Example 1, 1.2 ml of 2-hydroxyethyl methacrylate and 7.6 ml of triethyl borate were used for the production of the catalyst. The titanium content of the catalyst thus produced was 3.5 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

#### Example 4

In Step (ii) of Example 1, 1.2 ml of 2-hydroxyethyl methacrylate and 11.4 ml of triethyl borate were used for the production of the catalyst. The titanium content of the catalyst thus produced was 3.4 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

Example 5

In Step (ii) of Example 1, 1.2 ml of 2-hydroxyethyl methacrylate and 12.1 ml of tributyl borate were used for the production of the catalyst. The titanium content of the catalyst thus produced was 3.9 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

Example 6

In Step (ii) of Example 1, 1.2 ml of 2-hydroxyethyl methacrylate and 18.2 ml of tributyl borate were used for the production of the catalyst. The titanium content of the catalyst thus produced was 3.5 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

Example 7

In Step (ii) of Example 1, 1.2 ml of 2-hydroxyethyl methacrylate and 11.4 ml of triethyl borate were used, and in Step (iii) 40 ml of titanium tetrachloride and 20 ml of silicon tetrachloride were used for the production of the catalyst. The titanium content of the catalyst thus produced was 4.0 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

Example 8

In Step (ii) of Example 1, 1.2 ml of 2-hydroxyethyl methacrylate and 11.4 ml of triethyl borate were used, and in Step (iii) 20 ml of titanium tetrachloride and 40 ml of silicon tetrachloride were used for the production of the catalyst. The titanium content of the catalyst thus produced was 3.3 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

Comparative Example 1

In Step (ii) of Example 1, the catalyst was produced without 2-hydroxyethyl methacrylate or trimethyl borate. The titanium content of the catalyst thus produced was 3.9 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

Comparative Example 2

In Step (ii) of Example 1, 1.2 ml of 2-hydroxyethyl methacrylate was used alone, without trimethyl borate, for the production of the catalyst. The titanium content of the catalyst thus produced was 3.3 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

Comparative Example 3

In Step (ii) of Example 1, neither 2-hydroxyethyl methacrylate nor trimethyl borate was used, and in Step (iii) 60 ml of titanium tetrachloride was used for the production of the catalyst. The titanium content of the catalyst thus produced was 4.1 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

Comparative Example 4

In Step (ii) of Example 1, 1.2 ml of 2-hydroxyethyl methacrylate and 12.1 ml of tributyl borate were used, and in Step (iii) 60 ml of titanium tetrachloride was used for the production of the catalyst. The titanium content of the catalyst thus produced was 3.7 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

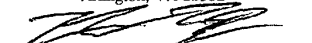






09/980505  
JC10 Rec'd PCT/PTO 27 NOV 2001

PATENT  
5333-02400

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A/CATALYST FOR ETHYLENE HOMO- AND CO- POLYMERIZATION

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## A CATALYST FOR ETHYLENE HOMO- AND CO-POLYMERIZATION

5    Technical Field

The present invention relates to a catalyst for homo-polymerization or co-polymerization of ethylene, or more particularly to a good-activity titanium solid complex catalyst supported in a carrier containing magnesium, said catalyst being capable of producing polymers of high bulk density with a narrow particle distribution and low contents of fine particles.

10

Background of the Invention

Catalysts containing magnesium for polymerization or co-polymerization of ethylene are known to have very good catalytic activities and to accord good bulk density, which are suitable for liquid-phase or gas-phase polymerization. By liquid phase polymerization of ethylene, it denotes the polymerization process performed in such medium of bulk ethylene, isopentane, or hexane, and as for the important characteristics of the catalyst used in the process, they are as follows: high activity, bulk density, the amount of molecules of low molecular weight dissolved in a medium, particle distribution of polymers, the amount of fine particles, and so on.

20       Many of the titanium-based catalysts containing magnesium for olefin polymerization, and the manufacturing methods thereof have been reported. Especially, many processes making use of magnesium solutions to obtain olefin polymerization catalysts of good bulk density have been known. There is a means of obtaining a magnesium solution by reacting magnesium compounds with such electron donors as alcohol, amine, cyclic ether, or organic carboxylic acid  
25   in the presence of a hydrocarbon solvent. As for the cases of use of alcohol, they are disclosed in US Patent Nos. 4,330,649, and 5,106,807. Further, the methods for production of catalysts containing magnesium by reacting a magnesium solution with a halogenated compound such as titanium tetrachloride are well known. Such catalysts provide good bulk density, but there is much yet to be improved with respect to their catalytic activity and bulk density. Meanwhile,  
30   when the polymerization is carried out by means of using such catalysts, the resultant polymers have large amounts of fine powder with a broad particle size distribution and low bulk density. As such, there are serious defects with respect to productivity and handling at the time of processing.

To solve these problems, US Patent Nos. 3,953,414 and 4,111,835 disclosed a process for making catalysts for production of globular polymers with a very large average particle size by means of spray-drying magnesium dichloride hydrates. These processes, however, require  
5 much production facilities for catalysts such as spray-drying equipment and others, and the resultant catalysts have the disadvantages of low activities. Further, due to the existence of very large particles in polymers, there may arise problems at the time of the melting process.

#### Summary of the Invention

10 As shown above, there is a need for the development of a new catalyst for homo-polymerization or co- polymerization of ethylene for producing polymers with the following conditions: simple manufacturing process, high polymerization activity, high bulk density for polymers by means of controlling the catalyst particles, and in particular narrow particle distribution with few fine particles. In the present invention, therefore, it is intended to provide a  
15 method for producing, from low-cost compounds via a simple process, a catalyst having an excellent catalytic activity, capable of producing polymers of high bulk density with narrow particle distribution and few fine particles. Further, the specific production process of catalysts and the steps thereof as disclosed in the present invention have never been reported in the prior art.

20 Consequently, the objective of the present invention is to provide a catalyst for homo-polymerization or co-polymerization of ethylene, said catalyst having good catalytic activity, capable of producing polymers of high bulk density, with narrow particle distribution and few fine particles.

25 Another objective of the present invention is to provide a simple process for producing a catalyst for homo-polymerization or co-polymerization of ethylene.

Still other objectives and the utility of the present invention will become bulk as references  
30 are made with respect to the following descriptions and the claims thereto.

### Detailed Description of the Preferred Embodiments

The catalyst of good catalytic activity, capable of producing polymers having narrow particle distribution and high bulk density with few fine particles as provided in the present invention, is produced by a simple yet efficient manufacturing process, which comprises (i)

5 preparing a magnesium solution by contact-reacting a halogenated magnesium compound, with an alcohol, (ii) reacting the same with an ester compound containing at least one hydroxy group and a boron compound containing an alkoxy group, and (iii) producing a solid titanium catalyst by adding a titanium compound and a silicon compound.

10 Types of halogenated magnesium compounds used in the present invention are as follows: di-halogenated magnesiums such as magnesium chloride, magnesium iodide, magnesium fluoride, and magnesium bromide; alkylmagnesium halides such as methylmagnesium halide, ethylmagnesium halide, propylmagnesium halide, butylmagnesium halide, isobutylmagnesium halide, hexylmagnesium halide, amylmagnesium halide, alkoxymagnesium halides such as  
15 methoxymagnesium halide, ethoxymagnesium halide, isopropoxymagnesium halide, butoxymagnesium halide, octoxymagnesium halide; and aryloxymagnesium halides such as phenoxymagnesium halide and methyl-phenoxymagnesium halide. Of the above magnesium compounds, two or more compounds can be used in a mixture. Further, the above magnesium compounds can be effectively used in the form of a complex compound with other metals.

20

Of the compounds listed above, some can be represented by a simple formula, but the others cannot be so represented depending on the production methods of magnesium compounds. In the latter cases, it can be generally regarded as a mixture of some of the listed compounds. For example, the following compounds can be used in the present invention: such compounds  
25 obtained by reacting magnesium compounds with polysilolxane compounds, silane compounds containing halogen, ester, or alcohol; and such compounds obtained by reacting magnesium metals with alcohol, phenol, or ether in the presence of halosilane, phosphorus pentachloride, or thionyl chloride. However, the preferable magnesium compounds are magnesium halides, especially magnesium chloride or alkylmagnesium chloride, preferably those having an alkyl  
30 group of 1 ~ 10 carbons; alkoxymagnesium chlorides, preferably those having 1 ~ 10 carbons; and aryloxymagnesium chlorides, preferably those having 6 ~ 20 carbons. The magnesium solution used in the present invention is made by dissolving the aforementioned compounds with

alcohol as a solvent in the presence or absence of a hydrocarbon solvent.

As to the types of hydrocarbon solvents used in the present invention, they include aliphatic hydrocarbons such as pentane, hexane, heptane, octane, decane, and kerosene; alicyclic hydrocarbons such as cyclobenzene, methylcyclobenzene, cyclohexane, and methylcyclohexane; aromatic hydrocarbons such as benzene, toluene, xylene, ethylbenzene, cumene, and cymene; and halogenated hydrocarbons such as dichloropropane, dichloroethylene, trichloroethylene, carbon tetrachloride, and chlorobenzene.

When a magnesium compound is converted into a magnesium solution, alcohol is used in the presence or absence of the aforementioned hydrocarbons. The types of alcohol include those containing 1 ~ 20 carbon atoms such as methanol, ethanol, propanol, butanol, pentanol, hexanol, octanol, decanol, dodecanol, octadecyl alcohol, benzyl alcohol, phenylethyl alcohol, isopropyl benzyl alcohol, and cumyl-alcohol, although alcohols containing 1 ~ 12 carbon atoms are preferable. The average size of a target catalyst and its particle distribution can vary according to the type of alcohol, the total contents, types of magnesium compounds, and the ratio of magnesium to alcohol, etc. Nevertheless, the total amount of alcohol required to obtain the magnesium solution is at least 0.5 mol per each mole of the magnesium compound, preferably about 1.0 ~ 20 mol, or more preferably about 2.0 ~ 10 mol.

The reaction of a magnesium compound with alcohol for producing magnesium solution is preferably carried out in the presence of hydrocarbon. The reaction temperature, while variable depending on the type and the amount of alcohol, is at least -25°C, preferably -10 ~ 200°C, or more preferably about 0 ~ 150°C. It is preferable to carry out the reaction for about 15 minutes ~ 5 hours, preferably for about 30 minutes ~ 4 hours.

Of the electron donors used in the present invention, the ester compounds containing at least one hydroxy group include unsaturated aliphatic acid esters having at least one hydroxy group such as, 2-hydroxy ethylacrylate, 2-hydroxy ethylmethacrylate, 2-hydroxypropyl acrylate, 2-hydroxypropylmethacrylate, 4-hydroxy butylacrylate, pentaerithritol triacrylate; aliphatic monoesters or polyesters containing at least one hydroxy group such as 2-hydroxy ethyl acetate, methyl 3-hydroxy butylate, ethyl 3-hydroxy butylate, methyl 2-hydroxy isobutylate, ethyl 2-

hydroxy isobutylate, methyl 3-hydroxy-2-methyl propionate, 2,2-dimethyl-hydroxy propionate, ethyl-6-hydroxy hexanoate, t-butyl-2-hydroxy isobutylate, diethyl-3-hydroxy glutarate, ethyl lactate, isopropyl lactate, butyl isobutyl lactate, isobutyl lactate, ethyl mandelate, dimethyl ethyl tartrate, ethyl tartrate, dibutyl tartrate, diethyl citrate, triethyl citrate, ethyl-2-hydroxy-caproate, diethyl bis-(hydroxy methyl)malonate; aromatic esters having at least one hydroxy group such as 2-hydroxy ethyl benzoate, 2-hydroxy ethyl salicylate, methyl-4-(hydroxy methyl) benzoate, methyl-4-hydroxy benzoate, ethyl-3-hydroxy benzoate, 4-methyl salicylate, ethyl salicylate, phenyl salicylate, propyl-4-hydroxy benzoate, phenyl-3-hydroxy naphthanoate, monoethylene glycol monobenzoate, diethylene glycol benzoate, triethylene glycol benzoate; alicyclic esters having at least one hydroxy group such as lactone, and others. The amount of the ester compound containing at least one hydroxy group should be 0.001 ~ 5 mol per mole of magnesium, or preferably 0.01 ~ 2 mol per mole of magnesium.

For the boron compound containing an alkoxy group, the other electron donor in the present invention, a compound having a general formula of  $BR^1_n(OR^2)_{3-n}$  (here,  $R^1$  represents a hydrocarbon having 1 ~ 20 carbons or a halogen element,  $R^2$  for a hydrocarbon having 1 ~ 20 carbons, and n for an integer of 0 ~ 2) is preferable. More specifically, it includes trimethyl borate, triethyl borate, tributyl borate, triphenyl borate, methylboron diethoxide, ethylboron diethoxide, ethylboron dibutoxide, butylboron dibutoxide, phenylboron phenoxide, diethylboron ethoxide, dibutylboron ethoxide, diphenylboron phenoxide, diethoxyboron chloride, diethoxyboron bromide, diphenoxyboron chloride, ethoxyboron dichloride, ethoxyboron dibromide, butoxyboron dichloride, phenoxyboron dichloride, and ethylethoxyboron chloride. The amount of such compound should be 0.005 mol per mole of magnesium, or more preferably 0.05 ~ 2 mol per mole of magnesium.

As for the temperature for the contact-reaction of a magnesium solution, an ester compound containing at least one hydroxy group, and an alkoxy boron compound, the temperature of 0 ~ 100°C is appropriate, or more preferably 10 ~ 70°C.

In the process, the catalyst particles are recrystallized by reacting the magnesium compound solution with a mixture of a liquid titanium compound of a general formula of  $\text{Ti}(\text{OR})_a\text{X}_{4-a}$  (R-stands for an alkyl group with 1 ~ 10 carbons; X for a halogen atom; and "a" for a

natural number of 0 to 4) and a silicon compound of a general formula of  $R_nSiCl_{4-n}$  (here R stands for hydrogen; or an alkyl, alkoxy, haloalkyl, or aryl group having 1 to 10 carbons; or a halosilyl or halosilyl alkyl group having 1 to 8 carbons;  $n = 0-3$ ). The types of titanium compounds which satisfy the general formula of  $Ti(OR)_aX_{4-a}$  include 4-halogenated titanium such as  $TiCl_4$ ,  $TiBr_4$ , and  $TiI_4$ ; 3-halogenated alkoxy-titanium such as  $Ti(OCH_3)Cl_3$ ,  $Ti(OC_2H_5)Cl_3$ ,  $Ti(OC_2H_5)Br_3$ , and  $Ti(O(i-C_4H_9))Br_3$ ; 2-halogenated alkoxy-titanium compounds such as  $Ti(OCH_3)_2Cl_2$ ,  $Ti(OC_2H_5)_2Cl_2$ ,  $Ti(O(i-C_4H_9))_2Cl_2$ , and  $Ti(OC_2H_5)_2Br_2$ ; and tetra-alkoxy titaniums such as  $Ti(OCH_3)_4$ ,  $Ti(OC_2H_5)_4$ , and  $Ti(OC_4H_9)_4$ . A mixture of the above titanium compounds can also be used in the present invention. However, the preferable titanium compounds are those containing halogen, or more preferably titanium tetrachloride.

The types of silicon compounds satisfying the above general formula of  $R_nSiCl_{4-n}$  include silicon tetrachloride; trichlorosilanes such as methyltrichlorosilane, ethyltrichlorosilane, phenyltrichlorosilane; dichlorosilanes such as dimethylchlorosilane, diethyldichlorosilane, diphenyldichlorosilane, and methylphenyldichlorosilane; monochlorosilanes such as trimethylchlorosilane; and a mixture of these silicon compounds can also be used in the present invention, or more preferably silicon tetrachloride can be used.

The amount of the mixture of a titanium compound and a silicon compound used during the re-crystallization of the magnesium compound solution is appropriately 0.1 ~ 200 mol per mole of the halogenated magnesium compound, preferably 0.1 ~ 100 mol, or more preferably 0.2 ~ 80 mol. The molar ratio of a titanium compound to a silicon compound in the mixture is appropriately 0.05 ~ 0.95, or more preferably 0.1 ~ 0.8. When the magnesium compound solution is reacted with the mixture of a titanium compound and a silicon compound, the shape and the size of the resultant re-crystallized solid constituents vary a great deal according to the reaction conditions. In order to obtain the target size of the catalyst and the size and distribution of the polymers, as intended by the present invention, it is advantageous to maintain the above mixture amounts for said titanium and silicon compounds, as well as their mix ratios. If it is outside of the above range, it will be difficult to obtain the results as intended. The reaction of the magnesium compound with the mixture of a titanium compound and a silicon compound should be carried out preferably at a sufficiently low temperature to result in formation of solid constituents. More preferably, the reaction should be carried out by contact-reaction at  $-70 \sim$



70°C, or most preferably at -50 ~ 50°C. After the contact-reaction the reacting temperature is slowly raised for sufficient reaction for the duration of 0.5 ~ 5 hours at 50 ~ 150°C.

The particles of the solid catalysts obtained during the above process can be further reacted with titanium compounds. These titanium compounds are titanium halides, and halogenated alkoxy titanium with an alkoxy functional group of 1 ~ 20 carbons. At times, a mixture of these compounds can also be used. Of these compounds, however, titanium halide and a halogenated alkoxy titanium compound having an alkoxy functional group of 1~8 carbons can be appropriately used, or more preferably titanium tetrahalide can be used.

Further, the solid complex titanium catalysts produced during the process of the present invention can be utilized during homo-polymerization or co- polymerization of ethylene. In particular, the catalyst is used in homo-polymerization of ethylene, and also in co-polymerization of ethylene and  $\alpha$  -olefin such as propylene, 1-butene, 1-pentene, 1-methyl-1-pentene, or 1-hexene having three or more carbons.

The polymerization reaction in the presence of the catalyst of the present invention is carried out by means of using (i) a solid complex titanium catalyst of the present invention, comprising magnesium, titanium, halogen, and electron donors, and (ii) a cocatalyst comprising compounds of organic metals of Groups II and III of the Periodic Table.

The solid complex titanium catalyst constituents of the present invention can be used in pre-polymerization of ethylene or  $\alpha$ -olefin prior to the use in the aforementioned polymerization reaction. The pre-polymerization can be carried out in the presence of a hydrocarbon solvent such as hexane, at a sufficiently low temperature, with ethylene or  $\alpha$ -olefin under pressure, in the presence of the above catalyst constituents and such an organic aluminum compound as triethylaluminum. Pre-polymerization, by maintaining the shape of the catalyst by surrounding the catalyst particles with polymers, is helpful in producing food-quality post-polymerization shape of the polymers. The weight ratio of the polymers to the catalysts after pre-polymerization is ordinarily 0.1 : 1 to 20 :1.

The organometallic compound in the present invention can be represented by a general formula of  $MR_n$ , wherein, M stands for a metal constituent of Group II or IIIA in the Periodic Table, such as magnesium, calcium, zinc, boron, aluminum, and gallium, R for an alkyl group with 1 ~ 20 carbons, such as a methyl, ethyl, butyl, hexyl, octyl, or decyl group, and n for the atomic value of the metal constituent. As for more preferable organometallic compounds, trialkyl aluminum having an alkyl group of 1 ~ 6 carbons, such as triethylaluminum and triisobutylaluminum, or the mixture thereof can be utilized. On occasions, an organic aluminum compound having one or more halogen or hydride groups, such as ethylaluminum dichloride, diethylaluminum chloride, ethyl-aluminum sesqui-chloride, or diisobutylaluminum hydride can also be used.

As for the polymerization reaction, it is possible to carry out either gas phase or bulk polymerization in the absence of an organic solvent, or liquid slurry polymerization in the presence of an organic solvent. These polymerization methods, however, are carried out in the absence of oxygen, water, or other compounds that may act as catalytic poison.

The concentration of the solid complex titanium compound (i) with respect to the polymerization system, in the case of a liquid phase slurry polymerization, is approximately 0.001 ~ 5 mmol in terms of the titanium atom of the catalyst per one liter of the solvent, or more preferably approximately 0.001 ~ 0.5 mmol. As for the solvent, the following compounds or the mixtures thereof can be used: alkanes or cycloalkanes such as pentane, hexane, heptane, n-octane, isooctane, cyclohexane, methylcyclohexane; alkylaromatic such as toluene, xylene, ethylbenzene, isopropylbenzene, ethyltoluene, n-propylbenzene, diethylbenzene; and halogenated aromatics such as chlorobenzene, chloronaphthalene, ortho-dichlorobenzene.

In the case of gas phase polymerization, the amount of the solid complex titanium catalyst (i) should be approximately 0.001 ~ 5 mmol in terms of the titanium atom of the catalyst per one liter of the polymerization reactant, preferably approximately 0.001 ~ 1.0 mmol, or more preferably approximately 0.01 ~ 0.5 mmol.

The preferable concentration of the organometallic compound (ii) is about 1 - 2,000 mol, as calculated by the aluminum atoms, per mole of the titanium atoms in the catalyst (i), or more

preferably about 5 ~ 500 mol.

To secure a good reaction rate of polymerization, the polymerization herein is carried out at a sufficiently good temperature, regardless of the polymerization manufacturing process.

5 Generally, the temperature of approximately 20 ~ 200°C is appropriate, or more preferably approximately 20 ~ 95°C. The appropriate pressure of monomers at the time of polymerization is the atmospheric to 100 atm, or more preferably 2 ~ 50 atm.

10 In the present invention, the changes in the molecular weight according to the amount of hydrogen at the time of polymerization are shown as a melt index (ASTM D 1238), the index generally known in the art. The value of the melt index generally becomes greater as the molecular weight decreases.

15 The products obtained by the method of polymerization of the present invention are solid ethylene homogeneous polymers or the copolymers of ethylene and  $\alpha$ -olefin, which have excellent bulk density and fluidity. Since the polymer yields are sufficiently good, there is no need for the removal of the catalyst residues.

20 The present invention is further described by means of the examples and comparative examples as below but should not be confined or limited to these examples.

#### Example 1

##### Production of catalyst

25 A solid complex titanium catalyst was produced by means of the following three steps:

##### (i) Step: Production of magnesium solution

30 Into a 1.0L reactor equipped with a mechanical stirrer, replaced with nitrogen atmosphere, 9.5 g of  $MgCl_2$  and 400 ml of decane were placed therein. After they were stirred at 300 rpm, 60 ml of 2-ethyl hexanol was added thereto. The temperature was

raised to 120 °C, and then the reaction was allowed to continue for three hours. The homogenous solution, which was obtained after the reaction, was cooled to room temperature (25°C).

- 5 (ii) Step : Contact-reaction of a magnesium solution, an ester containing a hydroxy group and an alkoxy boron compound

To the magnesium solution, cooled to room temperature as above, 1.2 ml of 2-hydroxyethyl methacrylate and 5.1 ml of trimethyl borate were added, and then the  
10 reaction was allowed to continue for an hour.

- (iii) Step : Treatment of a mixture of a titanium compound and a silicon compound

Into the above solution, a solution mixture of 30 ml of titanium tetrachloride and 30  
15 ml of silicon tetrachloride was dripped thereto for one hour at room temperature (25°C). After the completion of the dripping process, the temperature of the reactor was raised to 80°C while stirring, after which was maintained at that temperature for one hour. After stopping the stirring, the supernatant of the solution was removed, and to the remaining solid layer was added 300 ml of decane and 100 ml of titanium tetrachloride in sequence.  
20 There, the temperature was raised to 100°C and maintained thereat for two hours. After the reaction, the reactor was cooled to room temperature and the washing of the resulting solid product with 400ml of hexane was repeated until the removal of free unreacted titanium chloride. The titanium content of the solid catalyst so produced was 3.8%.

## 25 Polymerization

A 2-L good-pressure reactor was dried in an oven and assembled while still hot. In order to make the inside of the reactor nitrogen atmosphere, nitrogen and vacuum were alternatively manipulated three times in the reactor. To the reactor was added 1,000 ml of n-hexane, after which 2 mmols of triethylaluminum and a solid catalyst by 0.03 mmol in terms of  
30 the titanium atoms were added thereto. Then, 500 ml of hydrogen was added. The temperature was raised to 80°C while stirring at 700 rpm. The pressure of ethylene was

adjusted to 80 psi, and the polymerization was allowed to continue for an hour. After the polymerization, the temperature of the reactor was lowered to room temperature, and a large amount of ethanol was added to stop the polymerization. The polymer thus produced was collected by separation and was dried in an oven at 50°C for at least six hours, whereby polyethylene was obtained in the form of white powder.

The polymerization activity (kg of polyethylene divided by mmol of Ti) was calculated as the weight (kg) ratio of the polymer as produced per the amount of the catalysts so used (mmol of Ti). The results of the polymerization are shown in Table 1, together with the bulk density (g/ ml) of the polymers, the melt index (g/10 minutes), and particle size distribution of the polymers.

#### Example 2

In Step (ii) of Example 1, 1.2 ml of 2-hydroxyethyl methacrylate and 7.7 ml of trimethyl borate were used for the production of the catalyst. The titanium content of the catalyst thus produced was 3.4 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

#### Example 3

In Step (ii) of Example 1, 1.2 ml of 2-hydroxyethyl methacrylate and 7.6 ml of triethyl borate were used for the production of the catalyst. The titanium content of the catalyst thus produced was 3.5 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

#### Example 4

In Step (ii) of Example 1, 1.2 ml of 2-hydroxyethyl methacrylate and 11.4 ml of triethyl borate were used for the production of the catalyst. The titanium content of the catalyst thus produced was 3.4 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.



In Step (ii) of Example 1, the catalyst was produced without 2-hydroxyethyl methacrylate or trimethyl borate. The titanium content of the catalyst thus produced was 3.9 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

#### Comparative Example 2

In Step (ii) of Example 1, 1.2 ml of 2-hydroxyethyl methacrylate was used alone, without trimethyl borate, for the production of the catalyst. The titanium content of the catalyst thus produced was 3.3 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

#### Comparative Example 3

In Step (ii) of Example 1, neither 2-hydroxyethyl methacrylate nor trimethyl borate was used, and in Step (iii) 60 ml of titanium tetrachloride was used for the production of the catalyst. The titanium content of the catalyst thus produced was 4.1 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

#### Comparative Example 4

In Step (ii) of Example 1, 1.2 ml of 2-hydroxyethyl methacrylate and 12.1 ml of tributyl borate were used, and in Step (iii) 60 ml of titanium tetrachloride was used for the production of the catalyst. The titanium content of the catalyst thus produced was 3.7 %. The polymerization was carried out as in Example 1, and the results thereof are shown in Table 1.

Table 1 Results of Polymerization

Example	Activity (kg PE/ mmol Ti)	Bulk density (g/ml)	Melt Index (g/10min)	Distribution of Polymer Particles (wt %)							
				>1100 $\mu$ m	840 $\mu$ m	500 $\mu$ m	250 $\mu$ m	177 $\mu$ m	105 $\mu$ m	74 $\mu$ m	<44 $\mu$ m
1	5.4	0.38	0.52	0.6	3.4	10.8	52.4	21.2	8.4	2.6	0.6
2	4.8	0.36	0.43	0.4	9.4	16.4	45.2	18.7	6.7	3.2	0
3	6.3	0.40	0.58	0.2	1.2	12.6	58.2	24.8	2.6	0.4	0

4	5.9	0.38	0.42	0.3	4.6	9.3	54.8	19.8	6.7	4.5	0
5	6.4	0.37	0.54	0.8	4.6	8.6	59.4	18.6	7.1	0.9	0
6	5.4	0.36	0.52	0.5	4.1	10.5	52.8	20.2	11.7	0.7	0
7	6.2	0.35	0.54	0.2	0.7	16.4	41.4	36.8	1.2	2.1	1.2
8	6.0	0.35	0.52	1.2	12.1	26.2	38.4	19.4	1.5	0.4	0.8
CE 1	3.8	0.29	0.31	0	0.6	0.5	7.6	13.9	24.2	36.2	17.0
CE 2	4.4	0.26	0.42	2.2	2.7	2.4	9.4	13.7	12.6	34.2	22.8
CE 3	3.9	0.22	0.36	1.6	0.4	1.2	8.6	15.5	38.7	19.4	14.6
CE 4	3.6	0.28	0.31	0.7	3.8	5.1	16.2	32.4	22.1	15.5	4.2

\* CE : Comparative Examples

As shown above, the production process of the catalyst of the present invention for homo-polymerization and co-polymerization of ethylene is simple with excellent catalytic activity. Further, the polymers so produced have high bulk density and narrow particle distribution in addition to having the effect of reducing the amount of fine particles.



Claims

What is claimed is:

1. A solid titanium catalyst for homo-polymerization and co-polymerization of ethylene,  
 5 wherein said catalyst is produced by:
  - (i) preparing a magnesium compound solution by contacting a halogenated magnesium compound with alcohol;
  - 10 (ii) reacting said solution with an ester compound having at least one hydroxy group and a boron compound having an alkoxy group; and
  - (iii) reacting the solution from above(ii) with a mixture of a titanium compound and a silicon compound to produce solid catalyst, and optionally the solid catalyst are further  
 15 reacted with a titanium compound.
2. A solid titanium catalyst according to Claim 1, wherein said ester compound having at least one hydroxy group is an unsaturated aliphatic ester having at least one hydroxy group, which is selected from the group consisting of 2-hydroxy ethylacrylate, 2-hydroxy ethylmethacrylate, 2-hydroxy propyl acrylate, 2-hydroxy propylmethacrylate, 4-hydroxy butylacrylate, pentaerithritol triacrylate; an aliphatic monoester or polyester having at least one hydroxy group, which is selected from the group consisting of 2-hydroxy ethyl acetate, methyl 3-hydroxy butylate, ethyl 3-hydroxy butylate, methyl 2-hydroxy isobutylate, ethyl 2-hydroxy isobutylate, methyl 3-hydroxy-2-methyl propionate, 2,2-dimethyl-3-hydroxy propionate, ethyl-6-hydroxy hexanoate, t-butyl-2-hydroxy isobutylate, diethyl-3-hydroxy glutarate, ethyllactate, isopropyl lactate, butyl-isobutyl lactate, isobutyl lactate, ethyl mandelate, dimethyl ethyl tartrate, ethyl tartrate, dibutyl tartrate, diethyl citrate, triethyl citrate, ethyl-2-hydroxy-caproate, diethyl bis-(hydroxymethyl malonate; an aromatic ester having at least one hydroxy group, which is selected from the group consisting of 2-hydroxy ethyl benzoate, 2-hydroxy ethyl salicylate, methyl-4-(hydroxy methyl) benzoate, methyl-4-hydroxy benzoate, ethyl-3-hydroxy benzoate, 4-methyl salicylate, ethyl salicylate, phenyl salicylate, propy-4-hydroxy benzoate, phenyl-3-hydroxy naphthanoate, monoethylene glycol monobenzoate, diethylene glycol benzoate, triethylene glycol monobenzoate; an alicyclic ester having at least one hydroxy group as in hydroxy butyl-lactone; and wherein said boron compound having an alkoxy group is represented by the general formula  $BR^1_n(OR^2)_{3-n}$ ,  
 35

where  $R^1$  represents a hydrocarbon having 1 ~ 20 carbons or a halogen atom,  $R^2$  for a hydrocarbon having 1 ~ 20 carbons, and n for an integer of 0 ~ 2, said boron compound being selected from the group consisting of trimethyl borate, triethyl borate, tributyl borate, triphenyl borate, methylboron diethoxide, ethylboron diethoxide, ethylboron dibutoxide, butylboron dibutoxide, phenylboron diphenoxide, diethylboron ethoxide, dibutylboron ethoxide, diphenylboron phenoxide, diethoxyboron chloride, diethoxyboron bromide, diphenoxyboron chloride, ethoxyboron dichloride, ethoxyboron dibromide, butoxyboron dichloride, phenoxyboron dichloride, and ethylethoxyboron chloride.

3. A solid titanium catalyst according to Claim 1, wherein said titanium compound is represented by the general formula of  $Ti(OR)_aX_{4-a}$ , where R stands for an alkyl group with 1 ~ 20 carbons, X for a halogen atom, and "a" for an integer of 0 to 4; and wherein said silicon is represented by the general formula of  $R_nSiCl_{4-n}$ , where R stands for hydrogen, or an alkyl, alkoxy, haloalkyl, or aryl group having 1 to 10 carbons; a halosilyl or halosilyl alkyl group having 1 to 8 carbons; n = an integer of 0 to 4.

4. A solid titanium catalyst according to Claim 3, wherein said titanium compound is a 4-halogenated titanium, which is selected from the group consisting of  $TiCl_4$ ,  $TiBr_4$ , and  $TiI_4$ ; a 3-halogenated alkoxy titanium, which is selected from the group consisting of  $Ti(OCH_3)Cl_3$ ,  $Ti(OC_2H_5)Cl_3$ ,  $Ti(OC_2H_5)Br_3$ , and  $Ti(O(i-C_4H_9))Br_3$ ; a 2-halogenated alkoxy titanium, which is selected from the group consisting of  $Ti(OCH_3)_2Cl_2$ ,  $Ti(OC_2H_5)_2Cl_2$ ,  $Ti(O(i-C_4H_9))_2Cl_2$ , and  $Ti(OC_2H_5)_2Br_2$ ; and a tetraalkoxy titanium, which is selected from the group consisting of  $Ti(OCH_3)_4$ ,  $Ti(OC_2H_5)_4$ , and  $Ti(OC_4H_9)_4$ ; and wherein said silicon compound is a silicon tetrachloride; a trichlorosilane such as methyltrichlorosilane, ethyltrichlorosilane, and phenyl-trichlorosilane; a dichlorosilane such as dimethylchlorosilane, diethyldichlorosilane, diphenyldichlorosilane, and methylphenyldichlorosilane; and a monochlorosilane such as trimethylchlorosilane.

5. The solid titanium catalyst according to Claim 3, wherein said titanium compound comprises titanium tetrachloride, and said silicon compound comprises silicon tetrachloride.

6. The solid titanium catalyst according to Claim 1, wherein the amount of the mixture of a titanium compound and a silicon compound is 0.1 ~ 200 mol per mole of said halogenated magnesium compound, and the molar ratio of said titanium compound to said silicon compound in the mixture is 0.05 ~ 0.95.

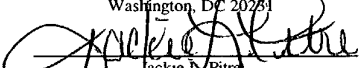
ABSTRACT

5        The present invention relates to a catalyst for homo-polymerization or co-polymerization of ethylene, or more particularly to a solid complex titanium catalyst for homo-polymerization or co-polymerisation of ethylene, said catalyst being produced by preparing a magnesium solution by contact-reacting a halogenated magnesium compound with alcohol, reacting said solution with an ester compound having at least one hydroxy group and a boron compound having an  
10    alkoxy group, and then reacting said solution with a mixture of a titanium compound and a silicon compound. The catalyst of the present invention has good activity, and the polymers produced by means of the catalyst herein has advantages in that the polymers have high bulk density with narrow particle distribution and a reduced amount of fines particles.

10 Rec'd PCT/PTO 29 MAR 2002 #4

IN THE UNITED STATES PATENT AND TRADEMARK OFFICE

§ Examiner: Unknown  
§ Group/Art Unit: Unknown  
§ Atty. Dkt. No: 5333-02400  
§

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By:  

Title: 

Date: March 12, 2002

ASSIGNMENT: x Enclosed for recording

**DECLARATION**

As a below named inventor, I hereby declare that:

My residence, post office and citizenship are as stated below next to my name.

I believe I am the original, first and sole inventor (if only one name is listed below) or the below named inventors believe they are the original, first and joint inventors (if plural names are listed below) of the subject matter which is claimed and for which a patent is sought on the invention entitled **A CATALYST FOR ETHYLENE HOMO- AND CO-POLYMERIZATION**, the specification of which:

- ☐ is attached herewith.  
☒ was filed on November 27, 2001 as Application Serial No. 09/980,505.

I hereby state that I have reviewed and understand the contents of the above identified specification, including the claims, as amended by any amendment referred to above.

I acknowledge the duty to disclose to the Patent and Trademark Office all information known to me to be material to patentability of the subject matter claimed in this application, as "materiality" is defined in Title 37, Code of Federal Regulations, § 1.56.

I hereby claim foreign priority benefits under Title 35, United States Code, § 119 of any foreign application(s) for patent or inventor's certificate listed below and have also identified below any foreign application for patent or inventor's certificate having a filing date before that of the application on which priority is claimed:

**PRIOR FOREIGN APPLICATION(S)**

			<u>Priority Claimed</u>
PCT/KR99/00638	Korea	October 23, 1999	Yes
(Number)	(Country)	(Date Filed)	
KR 1999/19193	Korea	May 27, 1999	Yes
(Number)	(Country)	(Date Filed)	

I hereby claim the benefit under Title 35, United States Code, § 120 of any United States application(s) listed below and, insofar as the subject matter of each of the claims of this application is not disclosed in the prior United States application in the manner provided by the first paragraph of Title 35, United States Code, § 112, I acknowledge the duty to disclose all information known to me to be material to the patentability of the subject matter claimed in this application, as "materiality" is defined in Title 37, Code of Federal Regulations, § 1.56, which become available between the filing date of the prior application and the national or PCT international filing date of this application:

N/A		Pending
(Application Serial No.)	(Filing Date)	(Status)
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(Application Serial No.)	(Filing Date)
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I hereby declare that all statements made of my own knowledge are true and that all statements made on information and belief are believed to be true; and further that these statements were made with the knowledge that willful false statements and the like so made are punishable by fine or imprisonment, or both, under Section 1001 of Title 18 of the United States Code and that such willful false statements may jeopardize the validity of the application or any patent issued thereon.

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